

An Efficient Acceleration of Solving Heat and Mass Transfer Equations with the Third Kind Boundary Conditions in Capillary Porous radially composite cylinder Using Programmable Graphics Hardware

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Abstract: *With the recent developments in computing technology, increased efforts have gone into simulation of various scientific methods and phenomenon in engineering fields. One such case is the simulation of heat and mass transfer equations which is becoming more and more important in analysing various scenarios in engineering applications. Analysing the heat and mass transfer phenomenon in different environments requires us to simulate it. However, this process of numerical solution of heat and mass transfer equation is very much time consuming. Therefore, this paper aims at utilizing one of the acceleration techniques developed in the graphics community that exploits a graphics processing unit (GPU) which is applied to the numerical solutions of heat and mass transfer equations. The nVidia Compute Unified Device Architecture (CUDA) programming model caters a good method of applying parallel computing to program the graphical processing unit. This paper shows a good improvement in the performance while solving the heat and mass transfer equations for capillary porous radially composite cylinder with the Third kind of boundary conditions numerically running on GPU. This heat and mass transfer simulation is implemented using CUDA platform on nVidia Quadro FX 4800 graphics card. Our experimental results depict the drastic performance improvement when GPU is used to perform heat and mass transfer simulation. GPU can significantly accelerate the performance with a maximum observed speedup of more than 7 fold times. Therefore, the GPU is a good approach to accelerate the heat and mass transfer simulation.*

Keywords: *Numerical Solution; Heat and Mass Transfer; General Purpose Graphics Processing Unit; CUDA.*

1. INTRODUCTION

During the last half century, many scientists and engineers working in Heat and Mass Transfer processes have put lots of efforts in finding solutions both analytically/numerically, and experimentally. To precisely analyze physical behaviors of heat and mass environment, to simulate several heat and mass transfer phenomena such as heat conduction, convection, and radiation are very important. A heat and mass transfer simulation is accomplished by utilizing parallel computer resources to simulate such heat and mass transfer phenomena. With the help from computer,

initially the sequential solutions were found, and later when high-end computers became available, fast solutions were obtained to heat and mass transfer problems. However, the heat and mass transfer simulation requires much more computing resources than the other simulations. Therefore, acceleration of this simulation is very essential to implement a practical heat and mass transfer simulation.

This paper utilizes the parallel computing power of GPUs to speed up the heat and mass transfer simulation. GPUs are very efficient considering theoretical peak floating-point operation rates [1]. Therefore, comparing with super-computer, GPUs is a powerful co-processor on a common PC which is ready to simulate a large-scale heat and mass transfer at a less resources. The GPU has several advantages over CPU architectures, such as highly parallel, computation intensive workloads, including higher bandwidth, higher floating-point throughput. The GPU can be an attractive alternative to clusters or super-computer in high performance computing areas.

CUDA [2] by nVidia already proved its effort to develop both programming and memory models. CUDA is a new parallel, C-like language programming Application program interface (API), which bypasses the rendering

Interface and avoids the difficulties from using GPGPU. Parallel computations are expressed as general-purpose, C-like language kernels operating in parallel over all the points in an application.

This paper develops the numerical solutions to Two-point Initial-Boundary Value Problems (TIBVP) of Heat and Mass Transfer with the Third kind boundary conditions in capillary porous radially composite cylinder. These problems can be found to have applications in drying processes, space science, absorption of nutrients, transpiration cooling of space vehicles at re-entry phase, and many other scientific and engineering problems. Although some traditional approaches of parallel processing to the solutions of some of these problems have been investigated, no one seems to have explored the high performance computing solutions to heat and mass transfer problems with compact multi-processing capabilities of GPU, which integrates multi-processors on a chip. With the advantages of this compact technology, we

developed algorithms to find the solution of TIBVP with the Third kind boundary conditions and compare with some existing solutions to the same problems. All of our experimental results show significant performance speedups. The maximum observed speedups are about 10 times.

The rest of the paper is organized as follow: Section II briefly introduces some closely related work; Section III describes the basic information on GPU and CUDA; Section IV presents the mathematical model of heat and mass transfer and numerical solutions to heat and mass transfer equations; Section V presents our experimental results; And Section VI concludes this paper and give some possible future work directions

2. RELATED WORK

The simulation of heat and mass transfer has been a very hot topic for many years. And there is lots of work related to this field, such as fluid and air flow simulation. We just refer to some most recent work close to this field here.

Soviet Union was in the fore-front for exploring the coupled Heat and Mass Transfer in media, and major advances were made at Heat and Mass Transfer Institute at Minsk, BSSR [3]. Later England and India took the lead and made further contributions for analytical and numerical solutions to certain problems. Narang [4-9] explored the wavelet solutions to heat and mass transfer equations and Ambethkar [10] explored the numerical solutions to some of these problems.

Krüger et al. [11] computed the basic linear algebra problems with the feathers of programmability of fragments on GPU, and further computed the 2D wavelets equations and NSEs on GPU. Bolz et al. [12] matched the sparse matrix into textures on GPU, and utilized the multigrid method to solve the fluid problem. In the meantime, Goodnight et al. [13] used the multigrid method to solve the boundary value problems on GPU. Harris [14, 15] solved the PDEs of dynamic fluid motion to get cloud animation.

GPU is also used to solve other kinds of PDEs by other researchers. Kim et al. [16] solved the crystal formation equations on GPU. Lefohn et al. [17] matched the level-set isosurface data into a dynamic sparse texture format. Another creative usage was to pack the information of the next active tiles into a vector message, which was used to control the vertices and texture coordinates needed to send from CPU to GPU. To learn more applications about general-purpose computations GPU, more information can be found from here [18]. Recently, Narang et al [19-21] have solved Heat and Mass Transfer simulation problems in solid, hollow and composite cylinders under different environmental conditions using GPU parallel processing environments.

3. AN OVERVIEW OF CUDA ARCHITECTURE

The GPU that we have used in our implementations is nVidia's Quadro FX 4800, which is DirectX 10 compliant. It is one of nVidia's fastest processors that support the CUDA API and as such all implementations using this API are forward compatible with newer CUDA compliant devices. All CUDA compatible devices support 32-bit integer processing. An important consideration for GPU performance is its level of occupancy. Occupancy refers to the number of threads available for execution at any one time. It is normally desirable to have a high level of occupancy as it facilitates the hiding of memory latency.

The GPU memory architecture is shown in figure 1.

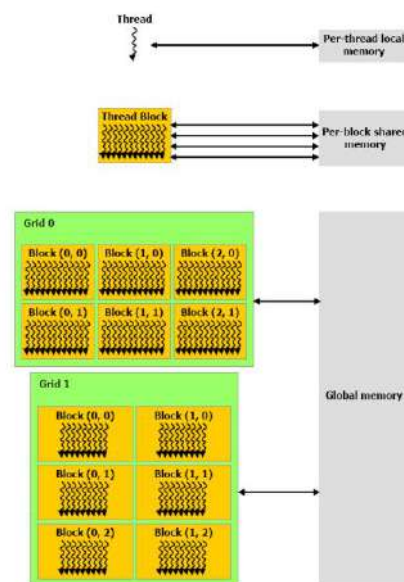


Figure 1: GPU Memory Architecture [2]

4. MATHEMATICAL MODEL AND NUMERICAL SOLUTIONS OF HEAT AND MASS TRANSFER

A. Mathematical Model

Consider the Heat and Mass Transfer through a capillary porous radially composite cylinder with boundary conditions of the third kind. Let the z-axis be directed upward along the capillary porous radially composite cylinder and the r-axis radius of the capillary porous radially composite cylinder. Let u and v be the velocity components along the z- and r- axes respectively. We have to write separate equations for each material as both will have different properties. Since we are concerned about studying the effect of conductivities of the 2 materials we observe their behaviour under the same initial and boundary conditions. So the first equation will correspond to the first material ($0 < z < 2L, 0 < r < a$) whereas the second equation correspond to the second material with different heat and mass constants ($0 < z < 2L, a < r < b$). Then the heat and mass transfer equations in the Boussinesq's approximation, are:

$$\frac{\partial T}{\partial t} = k_1 \left(\frac{\partial^2 T}{\partial r^2} + \frac{1}{r} \frac{\partial T}{\partial r} + \frac{\partial^2 T}{\partial z^2} \right) + k_2 \left(\frac{\partial C}{\partial t} \right) \quad (1)$$

$$\frac{\partial C}{\partial t} = k_3 \left(\frac{\partial^2 C}{\partial r^2} + \frac{1}{r} \frac{\partial C}{\partial r} + \frac{\partial^2 C}{\partial z^2} \right) + k_4 \left(\frac{\partial^2 T}{\partial r^2} + \frac{1}{r} \frac{\partial T}{\partial r} + \frac{\partial^2 T}{\partial z^2} \right) \quad (2)$$

$0 < z < 2L, 0 < r < a, t > 0$, where $a=0.5$, for the experimental simulation, and

$2L$ is the length of the first material For capillary radially composite porous composite cylinder.

$$\frac{\partial T}{\partial t} = k_{11} \left(\frac{\partial^2 T}{\partial r^2} + \frac{1}{r} \frac{\partial T}{\partial r} + \frac{\partial^2 T}{\partial z^2} \right) + k_{21} \left(\frac{\partial C}{\partial t} \right) \quad (1a)$$

$$\frac{\partial C}{\partial t} = k_{31} \left(\frac{\partial^2 C}{\partial r^2} + \frac{1}{r} \frac{\partial C}{\partial r} + \frac{\partial^2 C}{\partial z^2} \right) + k_{41} \left(\frac{\partial^2 T}{\partial r^2} + \frac{1}{r} \frac{\partial T}{\partial r} + \frac{\partial^2 T}{\partial z^2} \right) \quad (2a)$$

$0 < z < 2L, a < r < b, t > 0$, and $a=0.5$, and $b=1$, for experimental simulation

For capillary porous radially composite cylinder.

Initial Conditions

$$\begin{aligned} T(r, z, 0) &= 0 \\ C(r, z, 0) &= 1 \end{aligned} \quad (3)$$

Boundary Condition

$$\begin{aligned} T(r, 0, t) &= T_0 \\ C(r, 0, t) &= C_0 \end{aligned} \quad (4)$$

$$\begin{aligned} T(1, z, t) &= T_0 \\ C(1, z, t) &= C_0 \end{aligned} \quad (5)$$

At $z=0$

$$\begin{aligned} K_1(T(r, 0, t) - T_{2L}) &= k_h \frac{\partial T}{\partial r} \\ K_2(C(r, 0, t) - C_{2L}) &= k_m \frac{\partial C}{\partial r} \end{aligned} \quad (6)$$

At $r=1$

$$K_1(T(1, z, t) - T_{2L}) = k_h \frac{\partial T}{\partial r} \quad (7)$$

$$K_2(C(1, z, t) - C_{2L}) = k_m \frac{\partial C}{\partial r}$$

At $Z=2L$, it is assumed to have, infinity effect, where

Temperature and Concentration assume the environmental conditions i.e. ambient, temperature and concentration.

Since the radially composite cylinder is assumed to be capillary porous, μ_1 is the velocity of the fluid, T_p the temperature of the fluid near the capillary porous radially composite cylinder, T_∞ the temperature of the fluid far away from the capillary porous radially composite cylinder, C_p the concentration near the capillary porous radially composite cylinder, C_{2L} the concentration far end of the capillary porous radially composite cylinder, g the acceleration due to gravity, β the coefficient of volume expansion for heat transfer, β' the coefficient of volume expansion for concentration, ν the kinematic viscosity, σ the scalar electrical conductivity, ω the frequency of oscillation, k the thermal conductivity.

From Equation (1) we observe From Equation (1) we observe that v_1 is independent of space co-ordinates and may be taken as constant. We define the following non-dimensional variables and parameters.

$$t = \frac{t_1 V_0^2}{4\nu}, z = \frac{V_0 z_1}{4\nu} \quad (8)$$

$$u = \frac{u_1}{V_0}, T = \frac{T_1 - T_\infty}{T_p - T_\infty}, C = \frac{C_1 - C_\infty}{C_p - C_\infty}, P_r = \frac{\nu}{k}, S_c = \frac{\nu}{D}$$

$$M = \frac{\sigma B_0^2 \nu}{\rho V_0^2}, G_r = \frac{\nu g \beta (T_p - T_\infty)}{V_0^3}$$

$$G_m = \frac{\nu g \beta' (C_p - C_\infty)}{V_0^3}, \omega = \frac{4\nu \omega_i}{V_0^2}$$

Now taking into account Equations (5), (6), and (7) equations (1) and (2) reduce to the following form:

$$\frac{\partial T}{\partial t} + \frac{\partial^2 T}{\partial r^2} - 4 \frac{\partial C}{\partial t} + \frac{1}{r} \frac{\partial T}{\partial r} = \frac{4}{P_r} \frac{\partial^2 T}{\partial z^2} \quad (9)$$

$$\frac{\partial C}{\partial t} + \frac{\partial^2 C}{\partial r^2} - 4 \frac{\partial T}{\partial t} + \frac{1}{r} \frac{\partial C}{\partial r} = \frac{4}{P_r} \frac{\partial^2 C}{\partial z^2} \quad (10)$$

At $z=0$

$$K_1(T(r, 0, t) - T_{2L}) = k_h \frac{\partial T}{\partial r}$$

$$K_2(C(r, 0, t) - C_{2L}) = k_m \cdot \frac{\partial C}{\partial r} \quad (11)$$

At $r = 1$

$$K_1(T(1, z, t) - T_{2L}) = k_h \cdot \frac{\partial T}{\partial r}$$

$$K_2(C(1, z, t) - C_{2L}) = k_m \cdot \frac{\partial C}{\partial r} \quad (12)$$

B. Numerical Solutions

Here we sought a solution by finite difference technique of implicit type namely Crank-Nicolson implicit finite difference method which is always convergent and stable. This method has been used to solve Equations (8), and (9) subject to the conditions given by (4), (5) and (6). To obtain the difference equations, the region of the heat is divided into a grid or mesh of lines parallel to z and r axes. Solutions of difference equations are obtained at the intersection of these mesh lines called nodes. The values of the dependent variables T , and C at the nodal points along the plane $z=0$ are given by $T(0, t)$ and $C(0, t)$ hence are known from the boundary conditions.

In the figure 2, Δz & Δr are constant mesh sizes along z and r directions respectively. We need an algorithm to find single values at next time level in terms of known values at an earlier time level. A forward difference approximation for the first order partial derivatives of T and C . And a central difference approximation for the second order partial derivative of T and C are used. On introducing finite difference approximations for:

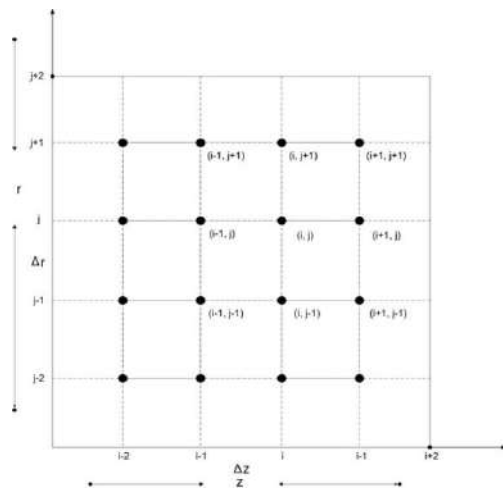


Figure 2: Finite Difference Grid for capillary porous radially composite cylinder

For the purposes of coming up with a numerical solution for the problem, the radius of the capillary porous radially composite cylinder is 1.0

$$\left(\frac{\partial^2 T}{\partial z^2}\right)_{i,j} = \frac{T_{i+1,j} - T_{i-1,j} + T_{i+1,j+1} - T_{i-1,j+1} - 2T_{i,j}}{2(\Delta z)^2}$$

$$\left(\frac{\partial^2 T}{\partial r^2}\right)_{i,j} = \frac{T_{i+1,j} - T_{i-1,j} + T_{i+1,j+1} - T_{i-1,j+1} - 2T_{i,j}}{2(\Delta r)^2}$$

$$\left(\frac{\partial T}{\partial r}\right)_{i,j} = \frac{T_{i+1,j} - T_{i-1,j} + T_{i+1,j+1} - T_{i-1,j+1}}{4(\Delta r)}$$

$$\left(\frac{\partial T}{\partial t}\right)_{i,j} = \frac{T_{i,j+1} - T_{i,j}}{\Delta t}, \left(\frac{\partial C}{\partial t}\right)_{i,j} = \frac{C_{i,j+1} - C_{i,j}}{\Delta t}, \left(\frac{\partial u}{\partial t}\right)_{i,j} = \frac{u_{i,j+1} - u_{i,j}}{\Delta t}$$

$$\left(\frac{\partial C}{\partial t}\right)_{i,j} = \frac{C_{i+1,j} - C_{i-1,j} + C_{i+1,j+1} - C_{i-1,j+1}}{4(\Delta t)}$$

$$\left(\frac{\partial^2 C}{\partial z^2}\right)_{i,j} = \frac{C_{i+1,j} - C_{i-1,j} + C_{i+1,j+1} - C_{i-1,j+1} - 2C_{i,j}}{2(\Delta z)^2}$$

$$\left(\frac{\partial^2 C}{\partial r^2}\right)_{i,j} = \frac{C_{i+1,j} - C_{i-1,j} + C_{i+1,j+1} - C_{i-1,j+1}}{2(\Delta r)^2}$$

$$\left(\frac{\partial C}{\partial r}\right)_{i,j} = \frac{C_{i+1,j} - C_{i-1,j} + C_{i+1,j+1} - C_{i-1,j+1}}{4(\Delta r)}$$

The finite difference approximation of Equations (8) and (9) are obtained with substituting Equation into Equations (8) and (9) and multiplying both sides by Δt and after simplifying, we let $\frac{\Delta t}{(\Delta z)^2} = r' = 1$ (method is

always stable and convergent), under this condition the above equations can be written as:

$$\frac{\partial C}{\partial t} = \frac{1}{2} \left(\frac{U + V - 2(T_{i,j} + C_{i,j})}{(\Delta r)^2} + \frac{U + V}{2r(\Delta r)} + \left(\frac{U + V - 2(T_{i,j} + C_{i,j})}{(\Delta z)^2} \right) \right)$$

$$\frac{\partial T}{\partial t} = \frac{1}{2} \left(\frac{2U + V - 2(2T_{i,j} + C_{i,j})}{(\Delta r)^2} + \frac{2U + V}{2r(\Delta r)} + \frac{2U + V - 2(2T_{i,j} + C_{i,j})}{(\Delta z)^2} \right)$$

Let $U = T_{i+1,j} - T_{i-1,j} + T_{i+1,j+1} - T_{i-1,j+1}$

Let $V = C_{i+1,j} - C_{i-1,j} + C_{i+1,j+1} - C_{i-1,j+1}$

C. Grid Structure and Heat Continuity Condition

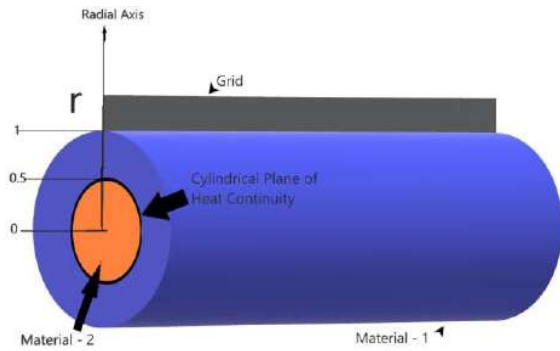


Fig. 3a: Plane of Heat Continuity in a Composite Solid Cylinder

The plane of heat and mass continuity (temperature, concentration, and their fluxes) is the plane along the radial axis of the solid radially composite cylinder (Shown in Fig 3-a and 3-b) where the material properties change i.e. where the two different materials are joined or merged together. So, the grid position in the above radially composite cylinder is as depicted in the figure 3b.

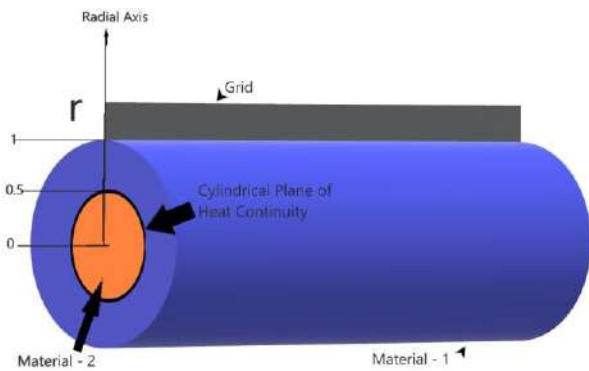


Fig 3b: Grid Arrangement in a Composite Solid Cylinder

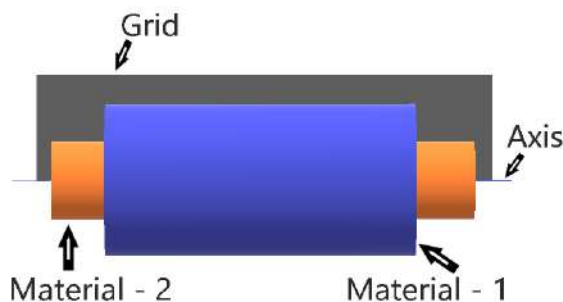


Fig. 3c: Grid Position in a Composite Solid Cylinder

At this point of interface between the two materials, i.e. the plane of heat continuity, when the heat transfer occurs, the temperature at the last grid point along any radius of the first material is approximately equal to the temperature at the first grid point in the second material. Similarly, the concentration at the last grid point along any radius of the first material is approximately equal to the concentration at the first grid point in the second material. So, the heat and mass continuity equation can be written as follows:

$$T_1(r, z_i, t) = T_2(r, z_0, t)$$

$$C_1(r, z_i, t) = C_2(r, z_0, t)$$

Similarly, fluxes continuity can be described by their first partial derivatives.

$$\frac{\partial T_1(r, z_i, t)}{\partial z} = \frac{\partial T_2(r, z_i, t)}{\partial z}$$

$$\frac{\partial C_1(r, z_i, t)}{\partial z} = \frac{\partial C_2(r, z_i, t)}{\partial z}$$

5. EXPERIMENTAL RESULTS AND DISCUSSION

A. Setup and Device Configuration

The experiment was executed using the CUDA Runtime Library, Quadro FX 4800 graphics card, Intel Core 2 Duo. The programming interface used was Visual Studio.

The experiments were performed using a 64-bit Lenovo Think Station D20 with an Intel Xeon CPU E5520 with processor speed of 2.27 GHZ and physical RAM of 4.00GB. The Graphics Processing Unit (GPU) used was an NVIDIA Quadro FX 4800 with the following specifications:

CUDA Driver Version:	3.0
Total amount of global memory:	1.59 Gbytes
Number of multiprocessors:	24
Number of cores:	92
Total amount of constant memory:	65536 bytes
Total amount of shared memory per block:	16384 bytes
Total number of registers available per block:	16384
Maximum number of threads per block:	512
Bandwidth:	
Host to Device Bandwidth:	3412.1 (MB/s)
Device to Host Bandwidth:	3189.4 (MB/s)
Device to Device Bandwidth:	57509.6 (MB/s)

In the experiments, we considered solving heat and mass transfer differential equations in capillary porous radially composite cylinder with boundary conditions of third kind using numerical methods. Our main purpose here was to obtain numerical solutions for Temperature T , and concentration C distributions across the various points in a capillary porous radially composite cylinder as heat and mass are transferred from one end of the capillary porous radially composite cylinder to the other. For our experiment, we compared the similarity of the CPU and GPU results. We also compared the performance of the CPU and GPU in terms of processing times of these results.

In the experimental setup, we are given the initial temperature T_0 and concentration C_0 at point $z = 0$ on

the capillary porous radially composite cylinder. Also, there is a constant temperature and concentration N_0 constantly working the surface of the capillary porous radially composite cylinder. The temperature at the other end of the capillary porous radially composite cylinder where $z = \infty$ is assumed to be ambient temperature (assumed to be zero). Also, the concentration at the other end of the capillary porous radially composite cylinder where $z = \infty$ is assumed to be negligible (≈ 0). Our initial problem was to derive the temperature T_1 and concentration C_1 associated with the initial temperature and concentration respectively. We did this by employing the finite difference technique. Hence, we obtained total initial temperature of $(T_0 + T_1)$ and total initial concentration of $(C_0 + C_1)$ at $z = 0$. These total initial conditions were then used to perform calculations.

For the purpose of implementation, we assumed a fixed length of the capillary porous radially composite cylinder and varied the number of nodal points N to be determined in the capillary porous radially composite cylinder. Since N is inversely proportional to the step size Δz , increasing N decreases Δz and therefore more accurate results are obtained with larger values of N . For easy implementation in Visual Studio, we employed the Forward Euler Method (FEM) for forward calculation of the temperature and concentration distributions at each nodal point in both the CPU and GPU. For a given array of size N , the nodal points are calculated iteratively until the values of temperature and concentration become stable. In this experiment, we performed the iteration for 10 different time steps. After the tenth step, the values of the temperature and concentration became stable and are recorded. We run the tests for several different values of N and Δz and the error between the GPU and CPU calculated results were increasingly smaller as N increased. Finally, our results were normalized in both the GPU and CPU.

B. Experimental Results

The normalized temperature and concentration distributions at various points in the capillary porous radially composite cylinder are depicted in Table 1 and Table 2 respectively. We can immediately see that, at each point in the capillary porous radially composite cylinder, the CPU and GPU computed results are similar. In addition, the value of temperature is highest and the value of concentration is lowest at the point on the capillary porous radially composite cylinder where the heat resource and mass resource are constantly applied. As we move away from this point, the values of the temperature decrease and concentration increase. At a point near the designated end of the capillary porous radially composite cylinder, the values of the temperature approach zero and concentration approach one.

TABLE 1. COMPARISON OF GPU AND CPU RESULTS FOR CAPILLARY POROUS RADIALLY COMPOSITE CYLINDER (CONCENTRATION)

Z	CPU RESULTS	GPU RESULTS
1	0.04785213	0.04012453
2	0.17820315	0.19687452
3	0.33654215	0.37812453
4	0.47896541	0.48961023
5	0.52310456	0.50745236
6	0.57850123	0.53321045
7	0.62035417	0.59610247
8	0.65874692	0.66375901
9	0.69874521	0.73241965
10	0.80214533	0.83845129
11	1	1

TABLE 2. COMPARISON OF GPU AND CPU RESULTS FOR CAPILLARY POROUS RADIALLY COMPOSITE CYLINDER (TEMPERATURE)

Z	CPU RESULTS	GPU RESULTS
1	1	1
2	0.79865412	0.76541258
3	0.70112453	0.71235402
4	0.61023562	0.64451236
5	0.54102036	0.52301452
6	0.51126548	0.49965874
7	0.43324175	0.46574123
8	0.37854698	0.33360125
9	0.33685421	0.30321525
10	0.26854721	0.28741005
11	0.16632148	0.16653241

Figure 4a and Figure 4b Shows the temperature and concentration distribution in the capillary porous radially composite cylinder with 4 different radiuses.

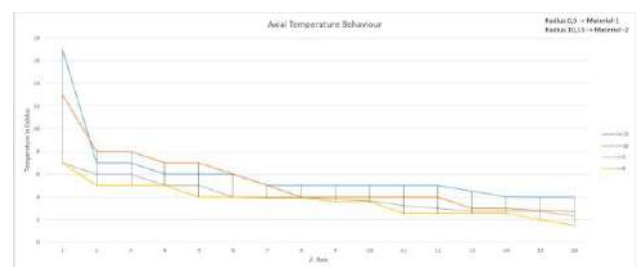


Figure 4a

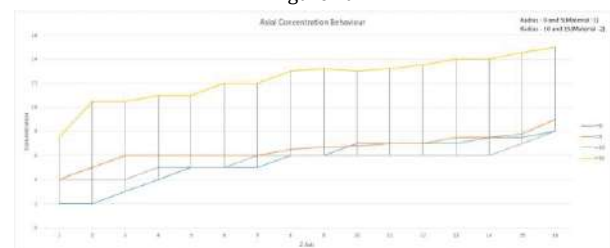


Figure 4b

Furthermore, we also evaluated the performance of the GPU (NVIDIA Quadro FX 4800) in terms of solving heat

and mass transfer equations by comparing its execution time to that of the CPU (Intel Xeon E5520).

For the purpose of measuring the execution time, the same functions were implemented in both the device (GPU) and the host (CPU), to initialize the temperature and concentration and to compute the numerical solutions. In this case, we measured the processing time for different values of N . The graph in Figure 5 depicts the performance of the GPU versus the CPU in terms of the processing time. We run the test for N running from 10 to 599 with increments of 30 and generally, the GPU performed the calculations a lot faster than the CPU.

- When N was smaller than 16, the CPU performed the calculations faster than the GPU.
- For N larger than 16 the GPU performance began to increase considerably

Figure 5a and 5b show some of our experimental results for both capillary porous radially composite cylinder.

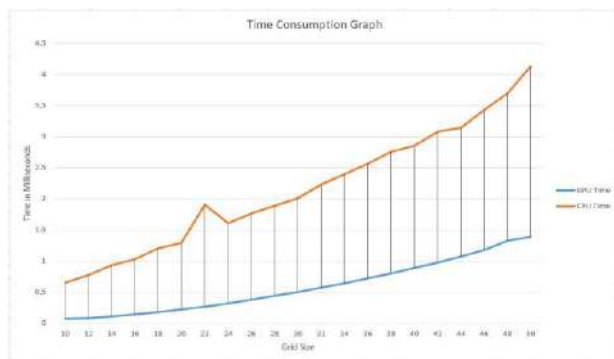


Figure 5a: Performance of GPU and CPU Implementations for capillary porous radially composite cylinder

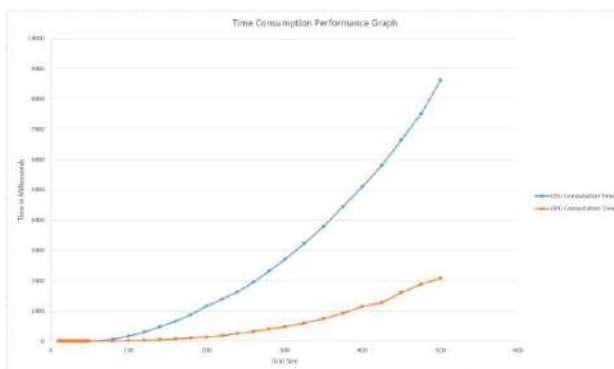


Figure 5b: Performance of GPU and CPU Implementations for capillary porous radially composite cylinder with incremental number of nodes

Finally, the accuracy of our numerical solution was dependent on the number of iterations we performed in calculating each nodal point, where more iteration means more accurate results. In our experiment, we observed that after 9 or 10 iterations, the solution to the heat and mass equation at a given point became stable.

For optimal performance, and to keep the number of iterations the same for both CPU and GPU, we used 10 iterations and experimental results for capillary porous radially composite cylinder show about 7 times speed-up.

6. CONCLUSION AND FUTURE WORK

We have presented our numerical approximations to the solution of the heat and mass transfer equation with the third kind of boundary and initial conditions for capillary porous radially composite cylinder using finite difference method on GPGPUs. Our conclusion shows that finite difference method is well suited for parallel programming. We implemented numerical solutions utilizing highly parallel computations capability of GPGPU on nVidia CUDA. We have demonstrated GPU can perform significantly faster than CPU in the field of numerical solution to heat and mass transfer. Experimental results for capillary porous radially composite cylinder indicate that our GPU-based implementation shows a significant performance improvement over CPU-based implementation and the maximum observed speedups are about 7 times.

There are several avenues for future work. We would like to test our algorithm on different GPUs and explore the new performance opportunities offered by newer generations of GPUs. It would also be interesting to explore more tests with large-scale data set. Finally, further attempts will be made to explore more complicated problems both in terms of boundary and initial conditions as well as other geometry

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